Open Channel Hydraulics

Prepared by

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CONTENTS

❑ Basics of Open channel/Free surface flow

- Introduction, practical application and difference between pipe and open channel flow
- Classification(boundary, geometry, shape)
- Geometrics properties
- Classification of flow in open channel

❑ Open channel is a conduit in which liquid flows with a free a

free surface under gravity.

Fig. 2: Schematic representation of Pipe flow and Free surface flow(open channel)

 $S \Rightarrow$

 $Y = 384 = 11$

4

Practical application

- It is a means of water transport
- For example Canal is used for Irrigation, drinking water supply
- Power canal, Drains, Sewer canal
- Navigation channel, Migration and survival of Aquatic lives, Channel is used for conveyance of sand , boulder etc.

Channel: Channel is a conduit made by nature it self to transport water. i.e., discharge has power to make channel shape and slope in order to flow downstream under the influence of gravity. **Canal:** All manmade conduits for water transport , Surface exposed to atmosphere, free surface flow **Here we include canal into Channel for their hydraulic studies purpose**.

Classification :

Rigid Boundary channel: whose beds and banks are fixed. For example : Power canal, Water supply canal etc.

Mobile Boundary Channel : The channel whose boundary changes.

For example : all natural channels i.e., rivers, streams etc.

Prismatic channel: Whose x-section and slope doesn't vary

Non-prismatic channel: Whose x-section and slope varies

Natural : Channel Artificial : Canal

.

Some Photographs:

Fig.2.: (1) Aerial view of Bheri river (Jajarkot) as Mobile boundary channels in gravel bed streams. Photographs (2) depicts same river as gravel bed channels whose banks are rocky

 $\mathcal I$

Fig.3 & 4: Photographs 3 and 4 (Kamla river ,Nepal) shows alluvial channel as mobile boundary channel

Fig.5 & 6: Photographs 5 is of Pakhar khola (Sindhupalchowk district) , boulder stream and figure 6 shows power canal of Sunkoshi HPP as Prismatic channel

Earthen canal(BIP, Bagmati Irrigation Project)

Fig. 11: Upper Ganga canal passes through Roorkee, India for Irrigation and drinking water supply, Irrigates agricultural land of UP and supplies water to Delhi for drinking

Qd = 250 (irrigation for 20 lakh hectares) + 50 (drinking water) = 300 m3/s Total Length= 292 Km

Geometric Properties Let us consider a Simple Section such as trapezoidal section of a canal

Flowing area $A = by +zy^2$ Top width $= b + zy + zy = b + 2zy$ Wetted perimeter P = b+ 2y $\sqrt{1+z^2}$

4

$$
\begin{aligned}\n\text{Hydraulic radius} &= A/P = (b'y + z'y^2) / (b + 2y\sqrt{1 + z^2}) \\
\text{Hydraulic mean depth} &= A/T = (by + zy^2) / (b + 2zy)\n\end{aligned}
$$

 \rightarrow Hydraulic Radius (R_h) or Hydraulic Diameter: It is the ratio of area of flow to wetted perimeter of a channel or pipe

$$
R_h = \frac{Area}{wetted perimeter} = \frac{A}{P}
$$

Note: hydraulic Radius gives us indication for most economical section. More the Rh more economical will be the section.

Area, A		Wetted Perimeter, P Hydraulic radius, R Top width, B Hydraulic depth, D			
B_oy ÷	$B_o + 2y$	$\frac{B_oy}{B_0+2y}$	B_o	\boldsymbol{y}	$\overline{\psi}$
$(B_o + sy)y$	$B_0 + 2y\sqrt{1 + s^2}$	$\frac{(B_o+sy)y}{B_o+2y\sqrt{1+s^2}}$	$B_o + 2sy$	$\frac{(B_o+sy)y}{B_o+2sy}$	$\frac{1}{s}$ $\frac{1}{\sqrt{2}}$
sy^2	$2y\sqrt{1+s^2}$	$\frac{sy}{2\sqrt{1+s^2}}$	2sy	0.5y	
$\frac{1}{8}(\theta - \sin \theta)D_o^2$	$rac{1}{2} \theta D_o$	$rac{1}{4}\left(1-\frac{\sin\theta}{\theta}\right)D_o$ $D_o\sin\frac{1}{2}\theta$		$(\frac{\theta-\sin\theta}{\sin\frac{1}{2}\theta})\frac{D_o}{8}$	D, ൹

Table 1-1. Properties of typical channel cross sections

Let θ be angle subtended by water level MN at center of circle. And PL= y be water depth in channel Area of flowing section, MLN= OMLN-OMN (triangle) = $r^2\theta/2$ - 1/2 (2MP $*$ OP) $=$ r²θ/2 - 1/2 (2 OM Sinθ/2 OM $\cos\theta/2$)

 $=$ r²(θ - sin θ)/2

 $= r^2\theta/2 - 1/2$ (2 r Sin $\theta/2$ cos $\theta/2$)

15

$$
A = \frac{D^2}{8} (\theta - \sin \theta)
$$

Similarly wetted perimeter, MLN = $r\theta = D\theta/2$ and also $\cos\theta/2 = OP/r = (OL-PL)/r = (r-y)/r = ((D/2)-y)/(D/2) = (1-2y/D)$

Rectangular desp channel $\frac{y}{b+2y}$ $R = \theta$ of β ‡ ა⊷յ 丈 $\overline{\mathcal{R}}$

Franquer Channel

FIG. 2-1. Geometric elements of a circular section.

 S_0 = Bed slope of channel S_w = water surface slope S_f = slope of TEL At uniform flow, $S_0 = S_w = S_f$

Flow Classification

- Steady and Unsteady flow
- Uniform and Nonuniform flow
- Gradually and Rapidly varied flow
- Super critical, critical and sub critical flow

 $\lambda_{\rm{max}}$

Gradually varied and Rapidly varied flow

Gradually varied flow : A steady nonuniform flow in a prismatic channel where flow depth changes gradually along length of channel .

For example: Back water curve behind dam/weir

Rapidly varied flow : In rapidly varied flow, change in water surface curvature is large within short length of channel.

Fig.11: photographs of Rapidly varied flow at weir and in a experimental flume

 $\mathbf{r} = -r\mathbf{q}$

Subcritical flow : When Froude number of flow is less than one. Fr<1, For example flows in most of the rivers are subcritical flow **Supercritical flow** : The flow having Froude number greater than one. Fr>1.

In order to examine whether the flow is subcritical or supercritical let us throw a stone in a flowing stream. If the ripple formed propagates in both upstream and downstream then the flow is subcritical. If the wave propagates only in downstream then the flow is supercritical.

Basic Equation for channel hydraulics

- Continuity equation
- Energy equation
- Momentum equation

 $V = C$ $\frac{v}{c}$ \tilde{z} $=$ cooked flow $\sqrt{\gamma}$ $U =$ coitcal vebcit V_{c} = $y_c = \omega k \omega$ $V_c =$ 79

Continuity equation

The net inflow in the control volume in time Δt ,

$$
\left[\left(Q - \frac{\partial Q}{\partial x} \frac{\Delta x}{2} \right) - \left(Q + \frac{\partial Q}{\partial x} \frac{\Delta x}{2} \right) \right] \Delta t = - \frac{\partial Q}{\partial x} \Delta x \Delta t \quad \dots \dots \dots \dots \dots \dots (1)
$$

Also the increase in volume of the element in time Δt ,

$$
\frac{\partial}{\partial t} (A \Delta x) \Delta t \tag{2}
$$

Equating (1) and (2), and dividing by $\Delta x \Delta t$,

 ∂Q ∂x + ∂A $\frac{\partial A}{\partial t} = 0$ (3) But Q= AU, then (3) becomes, ν $\partial (AU)$ ∂x + ∂A $\frac{\partial A}{\partial t} = 0$ (4) Further, A=by for rectangular channel, then eqn.(4) becomes,

$$
\frac{\partial (byU)}{\partial x} + \frac{\partial (by)}{\partial t} = 0
$$

or, $b \left(\frac{\partial (yU)}{\partial x} + \frac{\partial y}{\partial t} \right) = 0$ or, $\frac{\partial (yU)}{\partial x} + \frac{y\partial U}{\partial x} + \frac{\partial y}{\partial t} = 0$ (5)

For steady flow, $\frac{\partial A}{\partial t}$ $\frac{\partial A}{\partial t}$ =0, then equation (4) becomes,

$$
\frac{\partial (AU)}{\partial x} = \frac{\partial c}{\partial x}, \text{ thus Q=A1U1=A2U2=A3U3=\dots (6)
$$

- If q be the lateral in flow or outflow from control volume, then
- Eqn(4) becomes,

$$
\frac{\partial (AU)}{\partial x} + \frac{\partial A}{\partial t} = \pm q
$$

Energy Equation,

- Let us consider non-curvilinear flow of channel section, where
- pressure distribution can be assumed as hydrostatic.
- Applying energy equation at section (1) and (2)

$$
\frac{p_1}{\gamma} + Z_1 + \frac{v1^2}{2g} = \frac{p_2}{\gamma} + Z_2 + \frac{v2^2}{2g} + hf
$$

$v1^2$ $y_1 +$ = constant …………(3) $2g$ Equation (3) is known as specific energy equation $\sum_{n=1}^{\infty} a_n$ class $\int_{\mathcal{C}} a_n$ Bakemetel **Momentum equation**

Considering figure (a), The net force along the x-direction must be equal to change in momentum flux

 $\sum F_x = M_2$ -M₁

or, P1-P2-Ff-Fa+Wsin
$$
\theta
$$
 = $\rho Q(u_2 - u_1)$ (4)

Energy correction factor

In Ideal fluid, shear stress, τ at any section = 0 and thus flow velocity at each section of x-section becomes uniform.

But for real fluid, it varies at each part of cross section of channel as shown in fig below . Flow is nonuniform across section. In order to consider this nonuniformity in the calculation of kinetic energy and momentum flux , velocity term has to be multiplied with some factor.

Consider a channel of x-section area A, in which u is the velocity of elementary area da, then the total $\frac{1}{2}m\sqrt{\frac{m}{m}} = \frac{S\sqrt{N}}{N}$ $K.E. = \int_0^t$ $\int_{0}^{A} \rho u dA \frac{u^2}{2}$ 2 = 1 $\frac{1}{2} \int_{0}^{2}$ \overline{A} ρu^{\wedge} 3dA ….(1)

And KE using average velocity $U= m$ U^2 2 $= (\rho U A \times U^2)/2 =$ ρA U^3 2 ……..(2) Now α be KE correction factor, Then $\alpha = (\frac{1}{2})^2$ $\frac{1}{2} \int_0^2$ \overline{A} ρu^{λ} 3dA)/ $(\rho A \frac{U^3}{2})$ 2) $\alpha =$ 1 $\frac{1}{A}$ \int_0^2 \overline{A} ($\overline{\mathcal{U}}$ \boldsymbol{U} $)^3 dA$ (4) But $A = by$, then the above equation becomes $\alpha =$ 1 $\frac{1}{y}$ \int_0^y \mathcal{Y} (\overline{u} \boldsymbol{U}) ³ ……………………(5) 1 2 $\sqrt{4,\mu^3}$ For this typical river x-section, $\alpha =$ $u_1^3A1+u_2^3A2+u_3^3A3$ $\hat{U}^3(A1+A2+A3)$ …………..(6)

Momentum Correction factor,

Similarly momentum flux of elementary area dA= $(\rho u dA)u$

Now, over area $A = \int_0^1$ \overline{A} $\rho u^2 dA$ (7)

And with uniform velocity, momentum flux over area A

 $= \rho U^2 A \dots (8)$

 \boldsymbol{U}

If β be the momentum correction factor, then

$$
\beta = \frac{\int_0^A \rho u^2 dA}{\rho U^2 A} = \frac{1}{A} \int_0^A (\frac{u}{U})^2 dA
$$

A=by, then

$$
\beta = \frac{1}{y} \int_0^y (\frac{u}{U})^2 dy \quad(8)
$$
For discrete area (above figure)

 $\beta =$ $u_1^2A1+u_2^2A2+u_3^2A3$ $U^2(A1+A2+A3)$ ……(9). Thus our energy and momentum

equation becomes

$$
y_1 + \alpha_1 \frac{v1^2}{2g} = \text{constant} \dots \dots \dots (10)
$$

$$
M_2 - M_1 = \rho Q (\beta_2^{\star} u_2 - \beta_1^{\star} u_1) \dots (11)
$$

Fig. Typical velocity variation in open channel

$$
V_{av} = \frac{v_{0.2} + v_{0.8}}{2}
$$
 also, $V_{av} = k$ Vs (k=0.8-0.95)

つ

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 Ω

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Fig.13 & 14: Typical velocity profile in a channel and photographs 14 shows current meter used for velocity measurement in a stream, Panauti, Nepal

Receivers Velocity measurement with more advanced instruments, Acoustic Doppler Velocimeter at Hydraulics lab, IIT Single Roorkee **Transmitter**

Sampling Volume

Ultrasonic flow meter for discharge measurement in pipe (Hydraulics lab, IIT Roorkee)

Fig. 7 : Velocity variation in quasi steady state

 $\mathbf{u}\left(t\right)$ $+ u'(t)$ $=$ \overline{u} $+$ v' (t)
un turbulent fluctuation $v(t)$ $=$ \overline{v} mean

Instantaneous velocity of flow along x, y and z direction

Time average velocity at a point in a fluid flow is given as,

$$
\overline{u} = \frac{1}{T} \int_0^T u dt
$$

Mean velocity:

$$
\overline{u} = \int_{t}^{t+T} u(t) dt = \frac{1}{N} \sum_{i=1}^{N} u_i
$$

continuous record discrete, equi-spaced pts.

Turbulent Fluctuation:

$$
u'(t) = u(t) - \overline{u} \quad : continuous record
$$

$$
u'_i = u_i - \overline{u} \quad : discrete points
$$

Turbulence Strength:

$$
u_{\rm rms} = \sqrt{u'(t)^2} = \sqrt{\frac{1}{N} \sum_{i=1}^{N} (u'_i)^2}
$$

Velocity distribution in turbulent flow (Flow resistance equation)

Velocity distribution equation can be derived using relation of turbulent shear stress(Prandtl mixing length theory) and equation given by Nikuradse, i.e., l=ky where, k= von karman constant=0.4 (for details ,follow books)

$$
\tau = \rho l^2 \left(\frac{du}{dy}\right)^2
$$

Or, du = $\frac{1}{k} \frac{dy}{y} \sqrt{\frac{\tau_0}{\rho}}$, where, l=ky and $\sqrt{\frac{\tau_0}{\rho}} = u^*$ shear velocity

On integration both side, we get $u =$ u∗ \boldsymbol{K} loge (y)+C …………………………………………………….(1)

Applying boundary condition, at y' , $u=0$; y' is a small

distance from boundary up to which u=0 Finally we get equation (5)

```
\overline{\mathcal{U}}u_*= 5.75 log (y/y') ………………………………………..(2)
```


Hydrodynamically smooth and rough boundary

Fig.10:Schematic representation of smooth and rough boundary

For smooth surface $\frac{K_s}{s}$ $\frac{K_S}{\delta'} \leq 0.25$, and $\delta' =$ 11.6γ u_* ; For rough surface $\frac{K_s}{s}$ $\frac{K_S}{\delta'}\geq 6.0$; for smooth boundary, y' = $\delta'/107$ Where as for rough surface $y' = Ks/30$

Now combining equation (4) with smooth and rough surface parameters, we get,

$$
\frac{u}{u_*} = 5.75 \log \left(\frac{y u_*}{\gamma}\right) + 5.50 \quad \dots \dots \dots (5) \text{ (for smooth surface)}
$$
\n
$$
\frac{u}{u_*} = 5.75 \log \left(\frac{y}{Ks}\right) + 8.50 \quad \dots \dots \dots (6) \text{(for rough surface)}
$$
\n
$$
\text{V} \sim \text{logy}
$$
\n
$$
\text{V} \sim \text{logy}
$$

Keulegan used equation 5 and 6 ,for the derivation of flow resistance equation in terms of mean velocity for smooth and rough channels

$$
\frac{U}{u_*} = 5.75 \log \left(\frac{R u_*}{\gamma} \right) + 3.25 \quad \dots \dots \dots (7) \text{ (for smooth channels)}
$$

 \boldsymbol{U} u_* $= 5.75 \log(\frac{R}{K})$ Ks) +6.25 ……….(8)(for rough channels)

For boundary in transition surface, above equation can't be applied. So,

Einstein and Barbarossa has given a resistance equation for transition
surface. surface,

 \boldsymbol{U} u_* $= 5.75 \log \left(\frac{12.27 R x}{Kc} \right)$ Ks) …….(9) for transition boundary, where $x = f$ k_{S} ′ 49

Fig.Correction factor for viscous effects in logarithmic formula given by Einstein

Expression for shear stress at channel boundary in Uniform flow

Pressure distribution in open channel

 $\sqrt{2}$ $Q = \alpha_s + \alpha_n$
= $(\nu \frac{\partial \nu}{\partial s} + \frac{\gamma \nu}{\partial t})$ $2 = 39$ $=0$ $\frac{\partial u}{\partial t} = 0$ 24

Concau \bigcirc Comma $P = 5gh + 5(y^2/h)$ Commer Gainden $p = 8gh - 3(\frac{v}{r})h$

A spillway filip burnet has a sadins at 20 m. 97 the flow velocity at section $R-B$ is 20 mpl and the flow depth is 15m. compute the pressure intersity at point $\beta = 59h + 3(\sqrt{3})h$ $(5D5)(9.8) \times 15$ (v)

Flow rinkone Egn O chezy's formula Junitary How marings formula is Darry without forward $v = c$ $=$ A/p = $\frac{dy}{dt+y}$ S_{\circ} af unkam blow $S_{6} = S_{2} = S_{f}$ C = chery's compat 57

Some important flow resistance formula : Chezy, Manning's formula

The shear stress at boundary of channel $\tau_{\circ} = \gamma RS$..(1) and also,

Shear stress exerted at boundary can be written in terms of

surface drag force, Drag force = \mathbf{C}_d $A\rho u^2$ 2 , thus shear stress $\tau =$

$$
\frac{C_d \frac{A\rho u^2}{2}}{A} = C_d \frac{\rho u^2}{2} \dots (2), \text{ where A is wetted perimeter area of}
$$

channel

Equating 1 and 2 $W \rightarrow$ We get $u = C\sqrt{RS}$

Chezy's coefficient can be estimated using Kutter's formula (follow book)

$$
2\pi i \frac{\partial \phi^{(n)}}{\partial} \left\{\n\begin{array}{c}\n\alpha + \frac{\partial \phi^{(n)}}{\partial} \\
\alpha + \frac{\partial \phi^{(n)}}{\partial} \\
\beta + \frac{\partial \phi^{(n)}}{\partial} \\
\gamma + \frac{\partial \phi^{(n)}}{\partial
$$

 $S = c$ terms d del

Manning's Formula $\angle c = R^{1/2}$ $R^{1/6}$ $C=\frac{R}{A}$ ….. Derive Manning's formula \overline{n} Relationship between Darcy-weisbach friction factor, Chezy eqn and Manning's equation $u = c$ V Put C in Chezy equation $\sqrt{\frac{26}{9}}$ $U = \frac{R^{1/6}}{R}$ $*\sqrt{RS}$ \overline{n} Or , U = $\frac{1}{\infty}$ $R^{2/3}S^{1/2}$ \overline{n} $x = 2\mu$ Similarly from, $\frac{U}{U}$ 8 8 8g = $\frac{0}{f}$ or, U= U_{*} = RS U_* \overline{f} \overline{f} Thus, U= $\int_{-\epsilon}^{8g}$ 1 $R^{2/3}S$ (relations to be $RS +$ \overline{f} \widehat{n} remembered)

 $S^{\prime\prime}$ $A \times \frac{1}{\gamma}$ R^2 $\frac{2}{3}$ $= AV =$ $=\frac{1}{7}AR^{2/3}S^{1/2}$ Flost
Flain $cot f$ manoing's soughners ny V factor > Off Oblow dept ded & bank matinal $\binom{7}{1}$ Sediment content at flowing Trens J Stape \bigotimes

Variation de hydraulic sadius bith depth of town $\frac{v}{v}$ S Cralar Rectangu Finangular - Tropizoidad

- **Factors affecting M anning's n**
- **Conveyance**
- section factor of channel

$$
Q = AU = \frac{1}{n} AR^{2/3} S^{1/2}
$$

K= Conveyance (channel carrying capacity) = \boldsymbol{n} $AR^{2/3}$

Section factor,
$$
Z = AR^{2/3}
$$
,
Thus Q= $(Z S^{1/2})/n$
Z= Qn/ $S^{1/2}$

Section factor is a unique function of flow depth. i.e., $Z = f(y)$

, keeping width, discharge and slope of channel constant. There is only one value of depth of flow of channel from above figure and such depth is known as normal depth of flow.

 $3 = \frac{1}{h} A R^{1/3} s^{1/2}$ X-Sectional Poopes $g = \frac{1}{2} ar^{2}$ $Z = AR^{\gamma}$ $k=\frac{1}{2}\text{D}k^{\frac{1}{3}}$

Material	\boldsymbol{n}	
Metals		
Steel	0.012	
Cast iron	0.013	
Corrugated metal	0.025	
Non-metals		
Lucite	0.009	
Glass	0.010	
Cement	0.011	
Concrete	$0.013 -$	
Wood	0.012	
Clay	0.013	
Brickwork	0.013	
Gunite	0.019	
Masonary	0.025	
Rock cuts	0.035	
Natural streams		
Clean and straight	0.030	
Bottom: gravel, cobbles and boulders 0.040		
Bottom: cobbles with large boulders	0.050	

Table 4-1. Typical values* of Manning n

*Compiled from tables presented by Chow [1959].

Fig.: Establishment of Uniform flow in long channel **Fig.: Establishment of Uniform flow in long channel**

deptur 1 DX-Seekon Prof (1) T-160 resistance egh $L_{7}g=\frac{1}{7}AK^{\frac{1}{3}}s^{\frac{1}{3}}$ R vanes y for \Leftrightarrow x $\sqrt{\frac{1}{2}}$ M vairates P, V, Zo distribution

- **Normal Depth**
- **Critical depth**

• **Mild slope, Critical slope and Steep slope**

Control Section

Whenever we drop a stone/or splash hand in flowing stream , there will be formation of wave and it will travel either at downstream or us/ds both. The wave which travels in downstream only then such flow is called supercritical flow. Since velocity of wave C is lower than stream velocity. And such flow is controlled at upstream. i.e., it is able to regulate supercritical flow at upstream control section. For example sluice gate is a control structure which regulates flow at downstream and a certain depth and discharge relationship can be established at such section.

Similarly , when wave travels at upstream, then such flow is subcritical flow. i.e., celerity is higher than flow velocity. It is easy to control subcritical flow by placing structures at downstream end. i.e., to control upstream section of flow, we have to put structure at downstream section.

For example. Spillway , weir are control sections for upstream flow control. And there exist unique relationship for depth and discharge at these structures

H = Z+ Ycos θ + αv^2 /2g ……………………………..(1) for very small angle cos $\theta = 1$ and taking kinetic energy correction factor $\alpha = 1$ $H = Z + Y + v^2/2g$ considering channel bed as datum, then $Z=0$

 $E = Y + v^2/2g$ /2g …………………….(2)

Here, the term $E = y + y^2$ form E= Y+ V², called as specific Empy, interstant

We have $Splelli$ energy, $E = y + v^{2}y = y + \frac{g^{2}}{2g(gy)^{2}}$
 $E = y + \frac{p^{2}}{2g(y)^{2}} = \frac{9}{15}$ ar) $E-y = \frac{p^2}{2r}y^2$
ar) $(E-y)y^2 = \frac{p^2}{2r} =$ constant

Mathematically, we can prove that E-y curve has two asymptotics
(Argraphofes is a sime that a curve approaches, as it heads toward

Energy –depth diagram

 $E =$

let us consider a channel having discharge Q , q (as discharge Y per unit width). ،
رسم لاسي]
اسم لاسيا $E - 7$

 \triangleleft

If mehrs

carve

Subomitical

V super

 $7 = 0$

 y_{1}

 ϵ

 y_{3}

 E_{1}

 $\sqrt{372}$

 y_{ϵ}

 $T=\frac{45}{7}$ \overline{A} 本 \bigvee $C\left(\frac{1}{2}C\right)$ Jept Spelitil eph you"
Envry sill se <u>Leti von </u> $=$ $7 + 8^{2}$ $for min^m. E_j$ $\left(\frac{dA}{dy}\right)^{-2}$ $\frac{8}{29}$ $|f$ $\frac{g^{2}}{2z}$ (-2 A⁻³) $\frac{dA}{dx}$ $1 - 82$ 76

 $\frac{\alpha f}{\frac{V}{V}} = 1$ $F = 2$ $\frac{g}{\beta} = 2$ $= 1$ $\frac{6}{\sqrt{2}}$ y $\frac{v^{2}}{y^{2}} = 1 \Rightarrow \frac{Q^{2}}{y^{2}y^{2}} =$ $= 2$ $\frac{3}{79c*8^{2}4}$ $\frac{a}{\sqrt{2}}$ $\frac{a}{\sqrt{2}}$ $\frac{a}{\sqrt{2}}$ $\frac{a}{\sqrt{2}}$ $\frac{2}{3}$ $Y_{c} = \begin{pmatrix} 2^{e} \\ 2^{e} \end{pmatrix}$

Dimension less specific $E=y+\frac{y^{2}}{y^{2}}=\frac{y^{2}}{z^{2}}+\frac{z^{2}}{z^{2}}$ $5y_c = \frac{2^{e}}{2^{e}}$ $\frac{f}{y_c} = \frac{y}{y_c} + \frac{y_c}{2y^2 y_c}$ $y_c^3 = y_c^2$ $9\frac{E}{y_c} = \frac{y}{y_c} + \frac{y_c^2}{2y^2}$ $= \frac{1}{2} \left(\frac{y}{y} \right)$ $\overline{\mathcal{F}}_{c}$ = $\mathcal{F}(\frac{y}{y_{c}})$

Subcriti Supercriticed $Fif: Dimm$ sonless Specific E/y_c

Depth - Discharge diagram

 $E = y + \frac{y^2}{2y} = y + \frac{g^2}{39.05}$ $27A^{2}$ $E - y = \frac{Q^2}{2g} A^2$ \mathcal{N} $28r^{2}+(E-y)=8^{2}$ \mathcal{P} $\&$ = $\forall x \in \mathcal{Y}$ $\frac{a}{2}$ in equally $(i+y=0 \t A=0 \t B=0)$
as $y=\epsilon$, $B=0$

$$
g = A\sqrt{2} \sqrt{\frac{E-y}{E-y}}
$$
\n
$$
af y = 0 \quad jA = 0, g = 0
$$
\n
$$
f = \sqrt{\frac{2}{3}} \sqrt{\frac{27}{19}} = 2
$$
\n
$$
f = \sqrt{\frac{27}{19}} \sqrt{\frac{27}{19}} = 0
$$
\n
$$
f = \sqrt{27} \sqrt{\frac{27}{19}} = \sqrt{27} \sqrt{\frac{27}{19}} = 0
$$
\n
$$
f = \sqrt{27} \sqrt{\frac{27}{19}} = \sqrt{27} \sqrt{\frac{27}{19}} = 0
$$
\n
$$
f = \sqrt{27} \sqrt{\frac{27}{19}} = 0
$$
\n
$$
f = -y = \frac{A}{27} \text{ (i)}
$$

 $E = 3 + 8^2$ $29M^2$ $\frac{8^{2}}{2gA^{2}}$ 9 E asim ega $E-y = P_{27}$ bom egn (M) n $\frac{6}{2}$ 8^2 $\gamma\sqrt{\frac{8^{2}7}{9A^{3}}}$ = 1 => $Fv = 1$ danne an pass a maxim discharge at Thus Constant Sp. Energy

 $E = 5m$ $5=7+\frac{v^2}{2g}=7+g^2$ 2982 $\frac{8^{2}}{298^{2}y^{2}}$ $\sqrt{8^2}$ $\overline{9}$ $\frac{1}{2}$ \leq M - 3 \tilde{C} 7273218 $\left(\frac{2}{3}\right)$ $\frac{12}{1} = \frac{17}{1} = \frac{12}{1} = 12$ $y = y^2$

Conto) Section